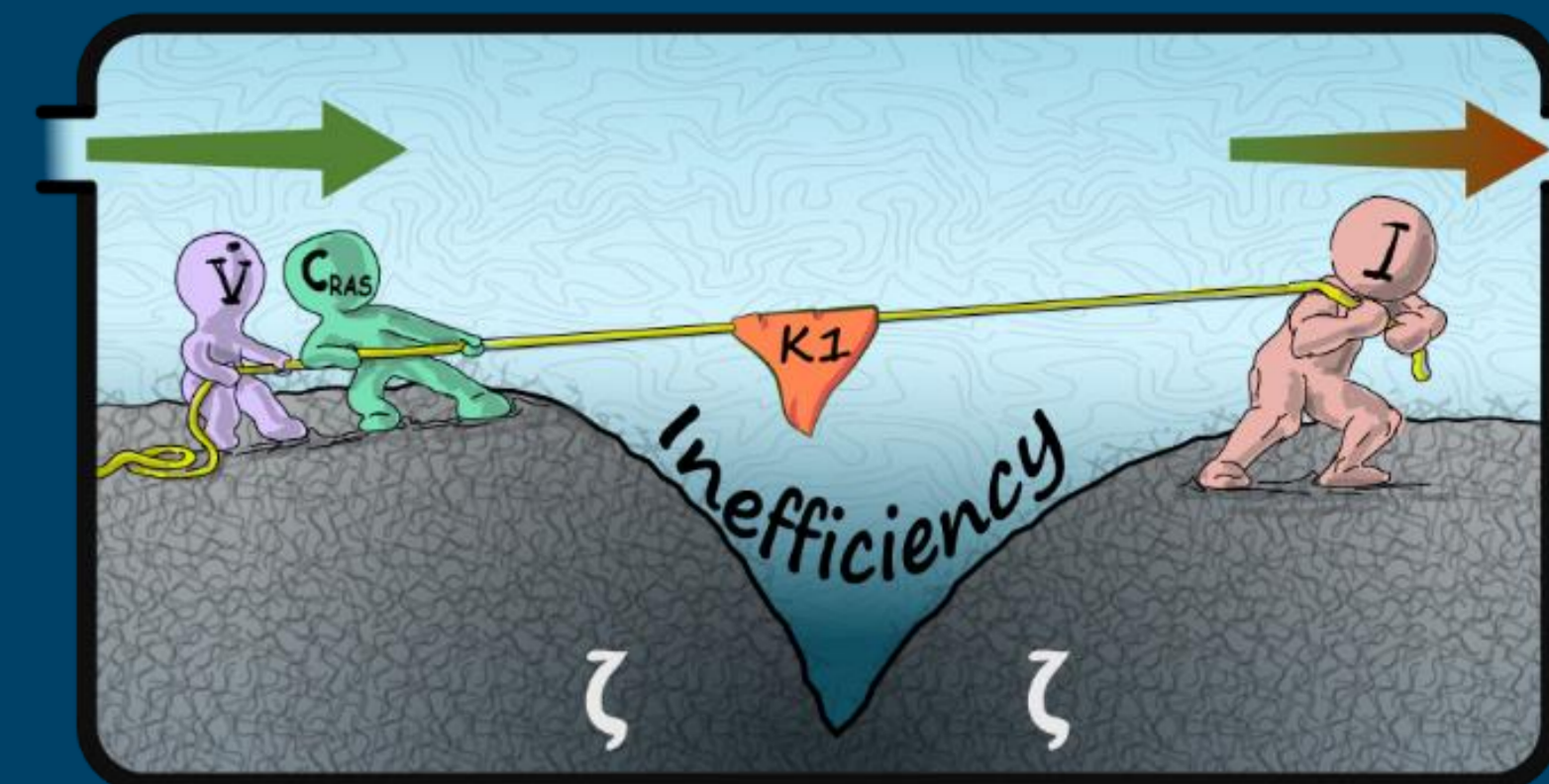




# Molar Fluxes and Cell Constants in Redox Flow Batteries – Identifying and Unifying RFB Cell Performance Criteria

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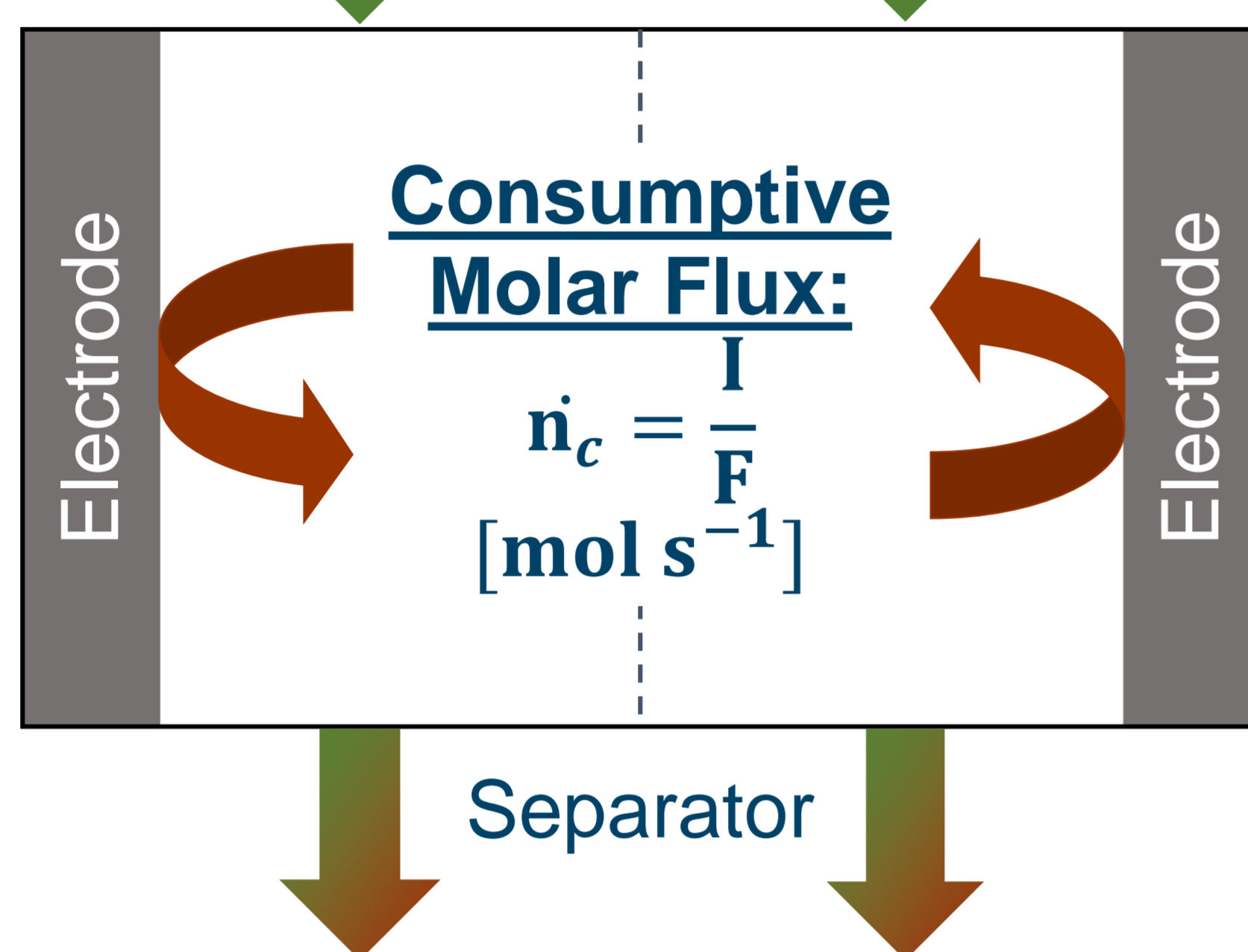
## Molar Fluxes

**Productive Molar Flux:**  
 $\dot{n}_p = c_{RAS} \cdot \dot{V} [\text{mol s}^{-1}]$

**Efficiency**

$$K1 = \frac{\dot{n}_p}{\dot{n}_c}$$

$$K1_{\text{critical}} = K1(90\% \eta_{\text{min}})$$



**Comparability**

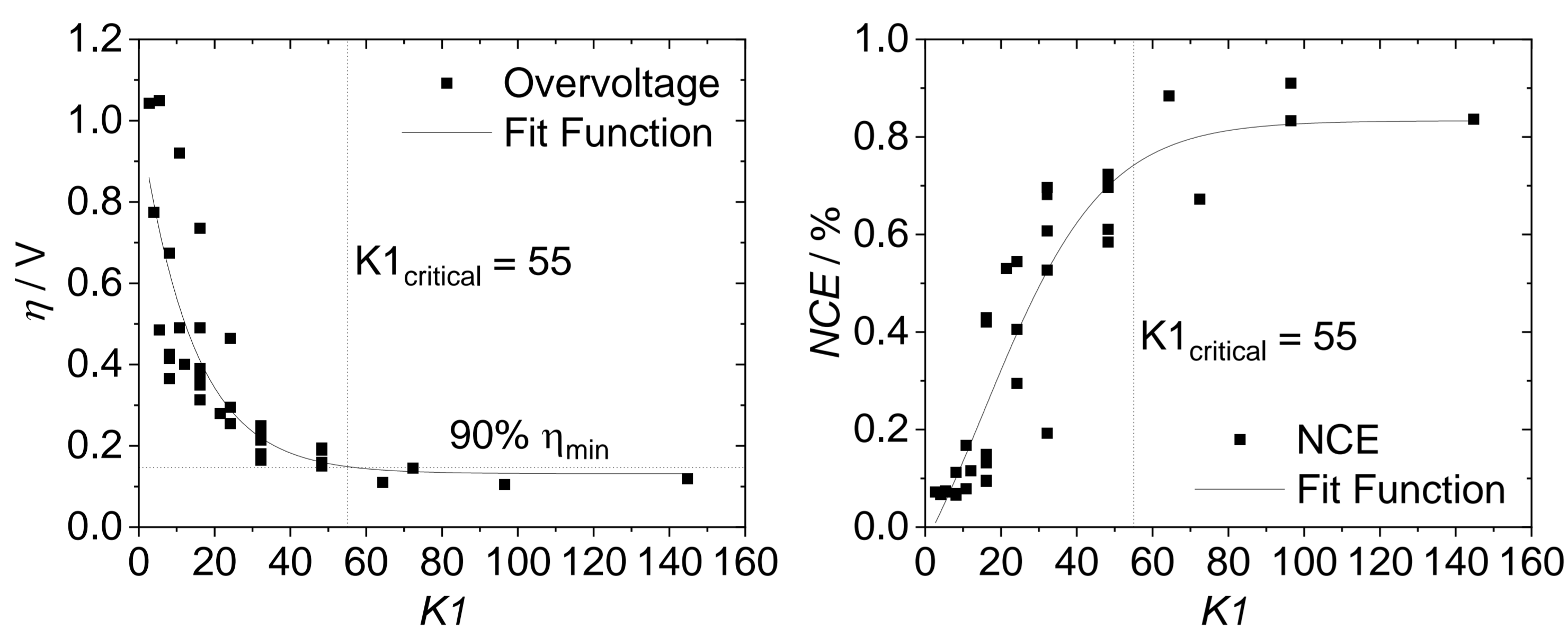
$$\zeta [\text{cm}^{-1}]$$

$$K2 = \frac{K1_{\text{critical}}}{\zeta} [\text{cm}]$$

|                              |                               |                       |
|------------------------------|-------------------------------|-----------------------|
| RAS                          | Redox Active Species          | -                     |
| $c_{RAS}$                    | RAS Concentration             | mol L <sup>-1</sup>   |
| $\dot{V}$                    | Volume Flow Rate              | L s <sup>-1</sup>     |
| $I$                          | Current                       | A                     |
| $F$                          | Faraday Constant              | A s mol <sup>-1</sup> |
| $\dot{n}_p$                  | Productive Molar Flux         | mol s <sup>-1</sup>   |
| $\dot{n}_c$                  | Consumptive Molar Flux        | mol s <sup>-1</sup>   |
| <b>K1</b>                    | RFB Operating Constant        | -                     |
| <b>K1<sub>critical</sub></b> | Critical Operating Parameters | -                     |
| $\zeta$                      | RFB Cell Constant             | cm <sup>-1</sup>      |
| <b>K2</b>                    | Comparability Constant        | cm                    |
| <b>NCE</b>                   | Normalized Charge Efficiency  | %                     |
| $\eta (\eta_{\text{min}})$   | (Minimum) Overvoltage         | V                     |

**K1** summarizes the operating parameters,  $\dot{n}_p$  and  $\dot{n}_c$ , of an RFB setup to determine the optimal ones by a simple experimental efficiency evaluation using  $\eta$  and **NCE**; **K2** and  $\zeta$  allow comparability between different RFB cell configurations by indicating the influence of a RFB configuration on its performance.

## Efficiency Evaluation



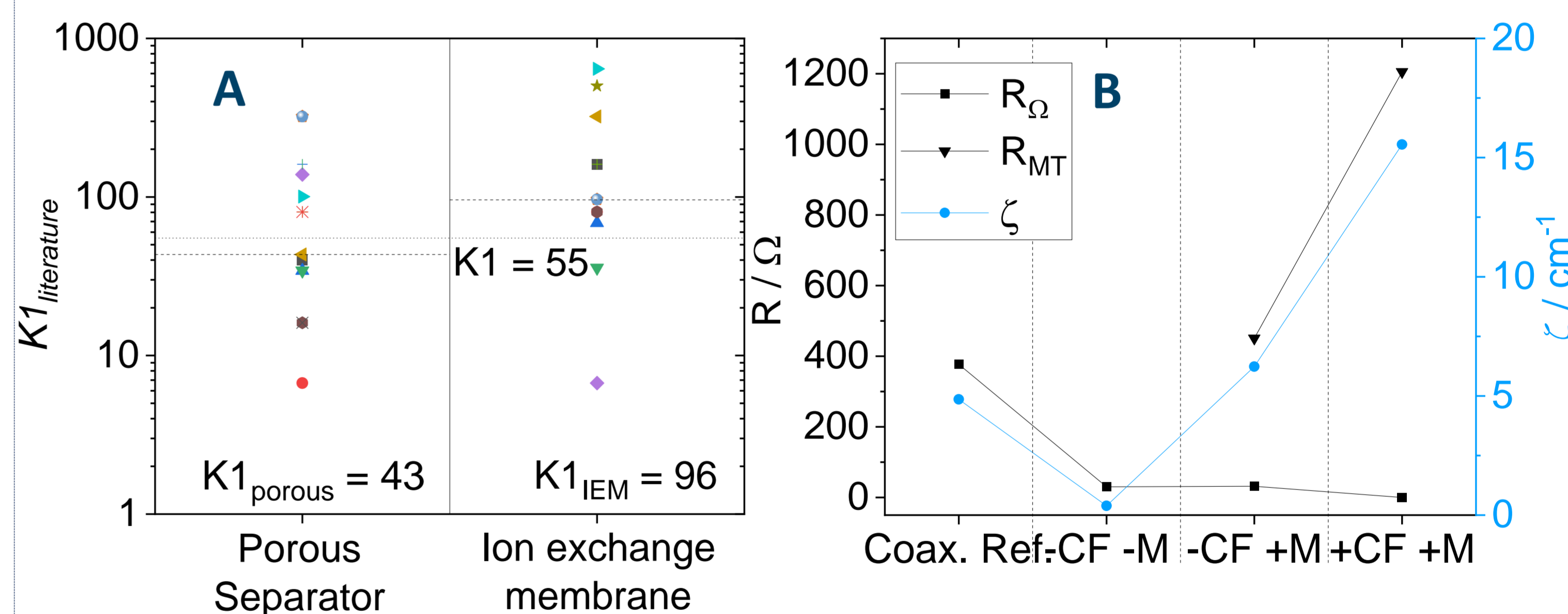
$\eta / \text{V}$  0.13

Overvoltage ( $\eta$ ) decreases with higher **K1** until minimum overvoltage ( $\eta_{\text{min}}$ )

**NCE** 74%

Normalized charge efficiency (**NCE**) increases with higher **K1** until real limited **NCE**

## Application of K1



**A** Literature **K1**  $K1_{\text{porous}} < K1_{\text{IEM}}$

Higher IEM penetration resistance requires larger compensating molar flux

**B** RFB Cell Constant  $\zeta$   $K2 = 3.5 \text{ cm}$

Mass transport through separator as the main limiting factor

## Standard Electrolyte

| Electrolyte Composition  | Operating Parameters  | Cell Configuration   |
|--|---|--|
| $\text{Fc} \rightleftharpoons \text{FcBF}_4$<br>0.3 M TBABF <sub>4</sub><br>Acetonitrile | $c_{RAS} = 5, 10, 15 \text{ mM}$<br>$\dot{V} = 5, 10, 20, 30 \text{ mL min}^{-1}$<br>$I = 5, 10, 15 \text{ mA}$ | 3D-printed RFB Cell <sup>[1, 2]</sup><br>Celgard® 2500 Separator |

## How to use Molar Fluxes?

1. Measure  $\zeta$  according to **ISO 7888** (0.1 M KCl) gradually increasing system complexity
2. Use **K2**  $\approx 3.5 \text{ cm}$  as first benchmark to estimate **K1<sub>critical</sub>**
3. Screen the cell performance and efficiency at different **K1** around **K1<sub>critical</sub>**
4. Calculate the real **K1<sub>critical</sub>** at 90% of  $\eta_{\text{min}}$
5. Recalculate **K2** using real **K1<sub>critical</sub>**

[1] L. Kortekaas, S. Fricke et al., A Digital Blueprint for 3D-Printing Lab-Scale Aqueous and Organic Redox-Flow Batteries, *Batteries & Supercaps* **2023**, e202300045  
[2] L. Kortekaas, S. Fricke et al., Building Bridges: Unifying Design and Development Aspects for Advancing Non-Aqueous Redox-Flow Batteries, *Batteries* **2022**, 9, 4